

The Significant Effect of Liquid Viscosity on Two-Phase Flow Pressure Gradient in Mini Channel with Slope of 15o against Horizontal

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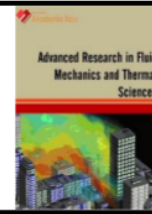
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The Significant Effect of Liquid Viscosity on Two-Phase Flow Pressure Gradient in Mini Channel with Slope of 15° against Horizontal

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ABSTRACT

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Two-phase flow is found in daily life as well as in the field of industry, which consists of three phases, namely liquid-solid, gas-liquid, and gas-solid. The fundamental characteristics of two-phase flow include flow pattern and flow pattern maps, void fraction, and pressure gradient. Some problems related to the pressure gradient comprise of the superficial velocity and viscosity of fluid mixture flow. This research discussed the significant effect of liquid viscosity in two-phase flow pressure gradient to find out the influence of liquid velocity, and also both superficial gas velocity (J_g) and liquid superficial velocity (J_l) on the pressure gradient. This research used a capillary pipe with a diameter of 1.6 mm. The fluid used was a gas-water mixture and glycerin with a concentration of 40%, 50%, 60%, and 70%. The pressure drop was measured using a pressure transducer and recorded by data acquisition. The result showed that the value of the two-phase flow pressure gradient was affected significantly by the number of liquid viscosity. The higher liquid viscosity leads to an increase in the two-phase flow pressure gradient. The pressure gradient was also affected either by liquid or gas superficial velocity, namely, the higher the superficial velocity of either by liquid or gas, the higher the pressure gradient.

Keywords:

concentration; gas-water; mini channel;
mixture; superficial; velocity

1. Introduction

Two-phase/component flows in the mini channel or capillary pipe is commonly implemented in daily life and also in the industrial sector. In daily life, two-component or multicomponent flow in a capillary pipe is applied in the blood flow system in the human body. In the industrial sector, two-phase flow in the capillary pipe is applied in the mini heat exchanger, mini evaporator, mini condenser, Micro Electro Mechanical System (MEMS), etc. The basic characteristics of two-phase flow in the capillary pipe are flow pattern or flow regime, flow pattern map, void fraction, pressure gradient or pressure drop. Many experiments have been conducted to study the two-phase flow. The

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studies that had been done by the researchers were generally using a pipe with normal and large size.

Fukano and Kariyaki [1] studied the characteristic of gas-water two-phase flow in a capillary pipe with a diameter of 1 mm, 2.4 mm, and 4.9 mm. Ali *et al.*, [2] showed the data of a study on pressure drop in the form of a friction factor of single-phase or two-phase. Triplett *et al.*, [3] conducted an experiment on void fraction and pressure drop that were caused by the friction of two-phase flow in a pipe with a diameter of 1.1 mm and 1.45 mm. Ju Lee, Han Yong Lee, Sang Lee and Lee [4] suggested a new correlation of pressure drop through a rectangular channel horizontal position with slit drop. Kawahara [5] conducted an experimental investigation on the characteristic of two-phase flow in a pipe with a diameter of 100 micrometers. Wongwises and Pipathatta [6] carried out an experiment on the flow pattern, pressure drop, and void fraction in the two-phase flow in a horizontal pipe, and mini slit annular channel slope with an outer diameter of 12.5 mm and an inner diameter of 8 mm. Saisorn and Wongwises [7] investigated the characteristics of two-phase flow, void fraction, and pressure drop in a micro circular channel with a diameter of 0.53 mm in a horizontal position. Barreto *et al.*, [8] studied the analysis on pressure drop and void fraction of two-phase flow in a microchannel. Abubakar *et al.*, [9] stated that the pressure gradient would increase as well as the increase of mixture viscosity. Gunawan *et al.*, [10] experimented with pressure difference in an acrylic pipe with an inner diameter of 26 mm. Meanwhile, an experimental study has also been carried out in the reduction of the friction pressure of two-phase flow on a microchannel with a diameter of 500 μm and a length of 0.5 m with a homogeneous and separate model. Several correlations exist of the two-phase flow viscosity and density used to predict the decrease in friction pressure. A comparison of predicted friction pressure drop shows that the correlation of Hibiki, Xuejiao, and Pamitran from separated models [11]. Sudarja *et al.*, [12] studied the pressure gradient of the two-phase flow of gas-water and glycerin 20% in a glass pipe with an inner diameter of 1.6 mm. Previous research has presented an analytical model for the calculation of two-phase pressure reduction using four refrigerants and test parameters namely vapor quality and mass flux. The pressure-drop model was examined with four coolants: R134a, R507A, R600a, and R1234xyh. The results show that there is a match between the two-phase pressure drop behavior for parameters that are fully variable compared to previous work so that this model can contribute to the design of heat exchangers and/or condensation tubes for other coolers [13]. To the best of the author's knowledge, the information on the pressure gradient in the capillary pipe with the variation of viscosity is still limited. Therefore, this study aims to obtain the information on the effect of superficial velocity and viscosity of the mixture of water-glycerin (40%, 50%, 60%, and 70%) against the pressure gradient in a horizontal capillary pipe with the slope of 15°.

2. Research Method

The used tool scheme in this study can be shown in Figure 1. This scheme consisted of some components, i.e., water tanks, water pumps, air compressors, pressure vessels, test sections, water traps, mixers, and connectors. The supporting tools used in this study were amplifiers, optical correction boxes, cameras, computers, video processing systems, and acquisition systems. The measurement tools used in this study were water flow meter, airflow meter, temperature indicator, thermocouple, pressure indicator, and pressure transducer. For streaming video shooting, a high-speed camera Nikon type J4 with a speed of 1200 fps and a resolution of 640 x 480 pixels was used. The data acquisition from "National Instrument" was used to convert data from analog to digital; then it could be recorded, stored, processed, and analyzed on a computer. The condition of this study

was adiabatic. The experiment was done in the superficial gas velocity (J_G) with an interval of 0.025 – 66.3 m/s, and the superficial liquid velocity (J_L) with the range of 0.033 – 4.935 m/s.

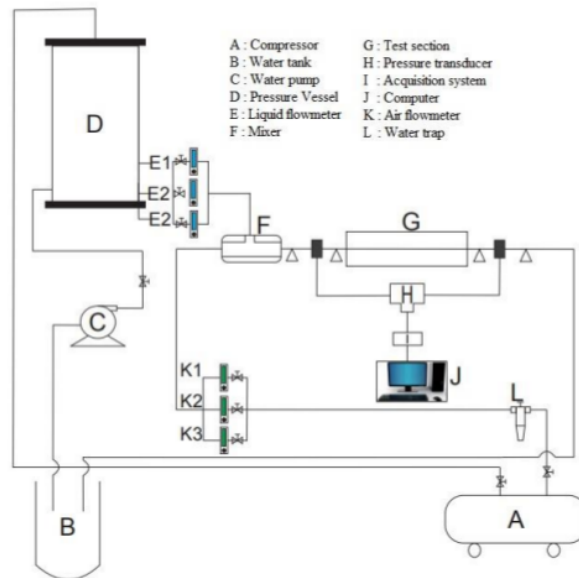


Fig. 1. Scheme of Research Installation

3. Result and Discussion

This study discussed the pressure drop per unit length (pressure gradient) two-phase flow in a capillary pipe with a diameter of 1.6 mm and the variation of viscosity and J_G - J_L . The variety of viscosity was done by providing the mixture with the glycerin percentage of 40%(GL40), 50%(GL50), 60%(GL60), and 70%(GL70). The data of the pressure gradient were taken by using the sensor of a pressure transducer (PT). After doing the research, it was obtained some data according to the variation of superficial gas velocity (J_G) and superficial liquid velocity (J_L). In addition to superficial velocity variations, variations in viscosity were also carried out in this study.

This study implemented the variation of superficial gas velocity (J_G) and superficial liquid velocity (J_L). This variation was done to obtain the effect that could occur because of the increase and decrease of superficial velocity on the pressure gradient. This study was done by using the variation of superficial velocity both for gas or liquid. This thing was done to show the effect of the change of the superficial velocity on the value of the pressure gradient in the capillary pipe with a diameter of 1.6 mm. Figure 2-3 shows the effect of superficial gas velocity (J_G) in the variation of superficial liquid velocity (J_L). The superficial velocity was measured by using the air and liquid rotameter with three range J_L (0.149; 0.879 and 2.297 [m/s]) and also by varying the J_G (0-66.3 [m/s]) in every J_L . Meanwhile, Figure 2-3 also shows the effect of J_L in the variation of J_G . Based on these data, it can be known that the pressure gradient ($\Delta P/\Delta Z$) is the function of J_G dan J_L . From these studies mentioned above, it can be seen that if the superficial gas velocity (J_g) increases, then the value of the pressure gradient will increase, as well as the superficial liquid velocity (J_L). Previously, Sudarja *et al.*, [14] had also conducted an experimental study on the adiabatic flow pattern of two-phase gas-liquid flow in mini-channel with inner diameters of 1.6 mm and the range of gas and liquid velocity were respectively 0.025 - 66.3 m / s and 0.033 - 4.935 m / s. Working fluids are used air and water-glycerine

solutions with various concentrations ranging from 20-60%. The research obtained data of bubbly, plug, slug-annular, annular, and churn flow patterns. It was also found that changes in liquid viscosity affect the shape of the flow pattern that occurs.

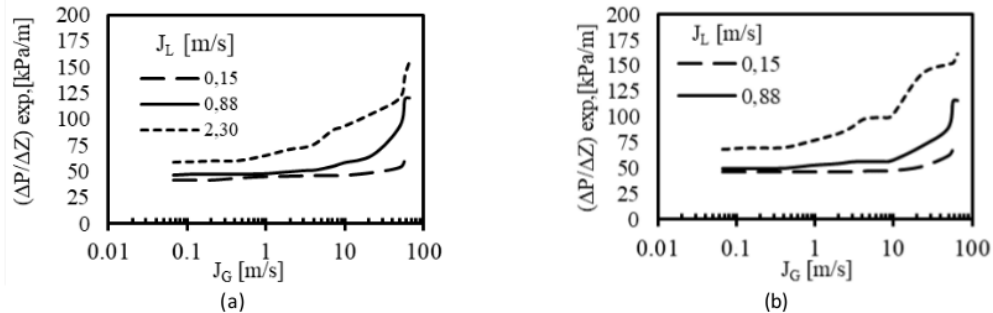


Fig. 2. Effect of J_G on pressure gradients with variations J_L on (a).GL40, (b). GL50

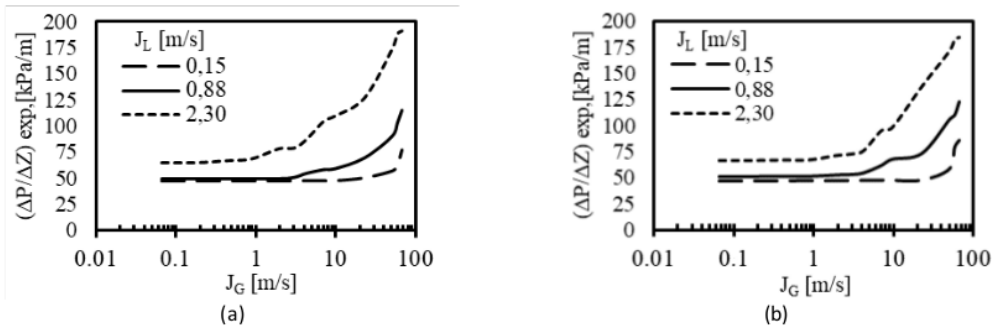


Fig. 3. Effect of J_G on pressure gradients with variations J_L on (a). GL60, (b). GL70

Meanwhile, Figure 4 shows that the viscosity of glycerin significantly affects the value of the pressure gradient. From the Figure, it can be seen that if the viscosity increases, then the value of the pressure gradient will increase as well. Research on the characteristics of two-phase oil-gas flow with high viscosity has been carried out to show some significant differences with the characteristics of low viscosity liquids. This experiment uses a 26 mm ID and 5.5 test tubes. m long horizontal pipes, with a variety of liquid viscosity from 1000. cP to 7500. cP. Superficial oil and gas velocity varies from 0.06. m / s to 0.5. m / s and starting at 0.3. m / s to 12.0. m / s respectively. The results of the study were compared with existing models and showed significant differences between liquids and gases with low and high viscosity[15]. In previous studies, there were also studies that focused on the effect of viscosity of fluids on the effect of entrances on vertical pipes with a diameter of 127 mm, gas superficial velocity varying between 0.01-5.40 m / s, superficial liquid velocity between 0.07-0.86 m / s, the viscosity is between 4.0 cP up to 104.6 cP. Vacuum fraction was measured using Electrical Capacitance Tomography and Wire Mesh Sensors, while differential pressure measurements using sensors [16]. On the other hand, experimental observations of fluid flow in the microchannel have been made for various variables. Experimental findings indicate changes in viscosity as a cause of deviation from conventional flow theory for macro channels. Based on an analysis of numerical friction factors, the entrance effect must be taken into account for any microfluidic system [17].

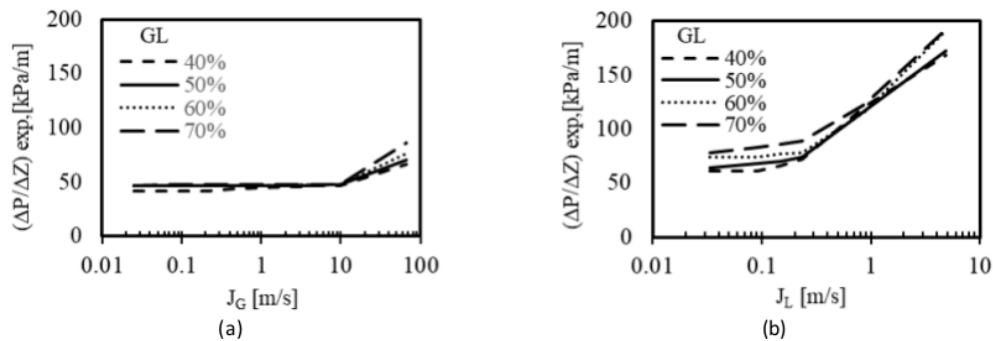


Fig. 4. The effect of fluid viscosity on pressure gradients on (a). J_L 0.149 m/s and J_G varies, (b) J_G 66.3 m/s and J_L varies

The value of the pressure gradient ($\Delta P/\Delta Z$) can also be seen in the time-series data. Figure 5 shows a pressure gradient against time at $J_G = 0.066$ [m / s] and $J_L = 0.7$ [m / s] for 0.5 seconds. The figure shows the mean pressure gradient is at 43.62 (GL40) and 48.78 kPa/m (GL70).

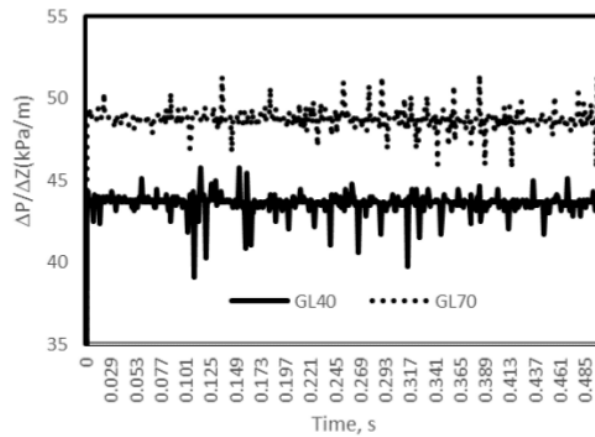


Fig. 5. Time series of pressure gradient at $J_G = 0.066$ [m/s] and $J_L = 0.7$ [m/s] GL40 and GL70

Figure 6 shows a graph of the pressure gradient probability density function at GL40 and GL70. From the two figures can be drawn physical meaning that the increase in viscosity, the pressure gradient will also increase. Recently, an experimental study of two-phase gas-liquid flow pressure gradients in a mini-channel (d_{in} 1.6 mm), superficial velocity of gases and liquids were in the range of 0.025-66,300 m / s and 0.033-4,935 m / s, respectively has concluded that the velocity of superficial gases and liquids is proportional to the pressure gradient[18]. Previous studies have also studied the flow of air-water in sharp 90 ° elbows for Reynolds numbers of 5600-12800. The results showed that the length of the upstream and downstream elbow disturbance a pressure drop were significantly affected by flow patterns[19]. The effects of vapor quality and internal diameter on a two-phase pressure drop were presented in previous studies with test equipment made of tubular stainless steel with an internal diameter of 1.70 mm and 1.224 mm and a length of 245 mm. Some general two-phase pressure reduction correlations suggested for macro and micro-scale channels are examined by comparing them with experimental data. None of the correlations examined agreed with this

research test data. A new correlation is proposed which is able to predict experimental data with MAD 16% and 86% data in the AE30% range[20]. The correlation effect of void fractions on the pressure gradient of two-phase water-air flow in vertical rectangular channels was investigated with superficial gas and liquid velocity ranging from 0.58 to 32 m / s and from 0.16 to 3.8 m / s. The results showed that the void fraction had a large influence on the pressure gradient on the slug flow pattern and churn flow but did not affect the bubble and annular flow. Furthermore, void fraction correlation has a smaller effect on the pressure gradient separation due to decreased channel size[21].

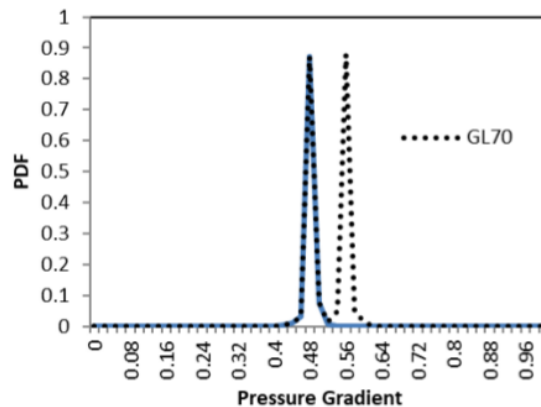


Fig. 6. Probability Density Function of pressure gradient at $J_G = 0.066$ [m/s] and $J_L = 0.7$ [m/s] (a) GL40, (b) GL70

4. Conclusion

Based on the research result that has been done in two-phase flow, it can be concluded that the superficial gas velocity (J_G) and superficial liquid velocity (J_L) significantly affect the value of the pressure gradient. The pressure gradient increases because of the effect of J_L with the range of 0.15; 0.88; 2.30 m/s and the variation of J_G 0-66.3 m/s. The pressure gradient also increases because of the impact of J_G in the range of 0.07; 7.00; 22.60 m/s and the variation of J_L 0.03-4.94 m/s. The viscosity of glycerin has a significant effect on the value of the pressure gradient. From the result of the research on the GL 40 %, 50%, 60%, and 70% with $J_G = 0.066$ [m/s] and $J_L = 0.7$ [m/s], it can be seen that the increase of pressure gradient value leads to the increase of glycerin viscosity.

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