

## Lampiran Tabel

### 1. 1. Data 1 Oktober 2014 (Pembebanan 100%, 100 MW )

**TABEL 1.1 DATA TERUKUR**

Tanggal : 1 Oktober 2014

Durasi : 1 Jam

Beban : 100 MW

NO.	Measuring point No.	Tag Number	Measuring Point	Unit	100%
			KWH transfer awal	MWh	3.980.630,0
			KWH transfer akhir	MWh	3.980.718,0
			KWH UAT PS awal	MWh	94.899,0
			KWH UAT PS akhir	MWh	94.908,0
1	E300	3MKA10CE001XV1	Generator watthour	kWh	97.000
2	E301	3MKA10CE009XV1	Generator Active Power	kW	100.557
3	E302	3MKA10CE003XV1	Generator Voltage	kV	12,74
4	E303	3MKA10CE006XV1	Generator Current	kA	6.036.22
5	E304	3MKA10CE012XV1	Generator power factor	-	0,99
6	E305	3MKA10CE011XV1	Generator Frequency	Hz	50,08
7	E306	3CBA10CE009XV1	Field (excitation) DC Voltage	V	232,92
8	E307	3CBA10CE010XV1	Field (excitation) DC Current	A	663,81
<b>FLOW</b>					
9	F520	3LCA30CF001XV1	LP No.1 Feedwater heater inlet condensate	t/h	311,15
10	F540	3LCA50CF001XV1	Dearator inlet condensate	t/h	302,37
11	F640	3HAC10CF001XV1	HP No.5 Feedwater heater outlet feedwater	t/h	301,33
12	F691	3LAE10CF001	SH1 Spray	t/h	14,89
13	F692	3LAE20CF001	SH2 Spray	t/h	22,39
14	F810	3LBG10CF001	Aux. Steam from SH after desuperheater	t/h	-
15	F900	3LCP62CF001XV1	Make-up water	t/h	2,26
<b>PRESSURE</b>					
16	P000	0QP10CP661	Atmospheric	hPa	1.004,07
17	P100	3LBA20CP010XV1	Main Steam	kg/cm <sup>2</sup> g	115,37
18	P105	3MAA10CP001XV1	Turbine Chamber	kg/cm <sup>2</sup> g	114,22
19	P110	3LBQ10CP001XV1	No. 1 Extraction Steam	kg/cm <sup>2</sup> g	33,35
20	P120	3LBQ20CP001XV1	No. 2 Extraction Steam	kg/cm <sup>2</sup> g	17,02
21	P130	3LBS30CP001	No. 3 Extraction Steam	kg/cm <sup>2</sup> g	7,40
22	P140	3LBS40CP001	No. 4 Extraction Steam	kg/cm <sup>2</sup> g	2,47
23	P150	3LBS50CP001	No. 5 Extraction Steam	kg/cm <sup>2</sup> g	(0,11)
24	P400	3MAG10CP011XV1	Turbine Exhaust	kg/cm <sup>2</sup> a	0,08

25	P510	3LCA20CP001XV1	Condensate Pump Discharge	kg/cm <sup>2</sup> g	15,43
26	P600	3LAA10CP001XV1	Deaerator Internal	kg/cm <sup>2</sup> g	5,14
27	P620	3LAB20CP001XV1	BFP discharge feedwater	kg/cm <sup>2</sup> g	171,29
28	P640	3HAC10CP001	HP No.5 Feedwater heater outlet feedwater	kg/cm <sup>2</sup> g	128,79
29	P800	3HAH72CP001	SH steam to HP aux. steam header	kg/cm <sup>2</sup> g	121,05
30	P810	3LBG10CP001	SH steam to HP aux. steam after desuperheater	kg/cm <sup>2</sup> g	17,11

**TABEL 1.2 DATA TEMPERATURE TERUKUR**

NO.	Measuring point No.		Measuring Point	Unit	100%
<b>TEMPERATURE</b>					
31	T000	LOCAL	Ambient	°C	-
32	T100	3LBA20CT003XV1	Main Steam	°C	535,14
33	T101	3LBA20CT001XV1	Main Steam (LOT3)	°C	534,84
34	T110	3LBQ10CT001XV1	No. 1 extraction steam	°C	392,43
35	T120	3LBQ20CT001XV1	No. 2 extraction steam	°C	290,01
36	T130	3LBS30CT001	No. 3 extraction steam	°C	210,08
37	T400	3MAG10CT001	Turbine exhaust	°C	40,39
38	T480	3PAB50CT001XV1	Condenser Inlet cooling water A	°C	30,18
39	T481	3PAB60CT001XV1	Condenser Inlet cooling water B	°C	30,19
40	T490	3PAB51CT001XV1	Condenser outlet cooling water A	°C	37,41
41	T491	3PAB61CT001XV1	Condenser outlet cooling water B	°C	37,43
42	T500	3LCA10CT001XV1	Condenser outlet condensate	°C	43,01
43	T525	3LCJ10CT001XV1	LP No. 1 feedwater heater drain	°C	53,02
44	T530	3LCA40CT001XV1	LP No. 2 feedwater heater inlet condensate	°C	93,88
45	T535	3LCJ20CT001XV1	LP No. 2 feedwater heater drain	°C	100,46
46	T540	3LCA50CT001XV1	Deaerator Inlet Condensate	°C	134,17
47	T600	3LAA10CT001XV1	Deaerator Internal	°C	171,18
48	T620	3LAB20CT001XV1	BFP discharge feedwater	°C	174,54
49	T625	3LCH40CT001XV1	HP No. 4 feedwater heater drain	°C	206,59
50	T630	3LAB30CT001XV1	HP No. 5 feedwater heater inlet feedwater	°C	201,00
51	T635	3LCH50CT001XV1	HP No. 5 feedwater drain	°C	208,61
52	T640	3LAB40CT001XV1	HP No. 5 feedwater heater outlet feedwater 1	°C	234,93
53	T641	3HAC10CT001	HP No. 5 feedwater heater outlet feedwater 2	°C	236,02

54	T800	3HAH72CT002XV1	SH steam to HP aux. steam header	°C	463,75
55	T810	3LBG10CT001	SH steam to HP aux. steam after desuperheater	°C	320,22
56	T900	3LCP11CT001XV1	Make-up water	°C	35,54

**TABEL 1.3 PERHITUNGAN ENTHALPHI**

Tanggal : 1 Oktober 2014

Durasi : 1 Jam

Beban : 100 MW

No.	ITEM	SYMBOL	UNIT	100%	
1	Main Steam	Press.	P100	kg/cm <sup>2</sup> a	116,40
2		Temp.	T100,T101	°C	535,14
3		Enthalpy	$h_{ms}$	kcal/kg	824,03
4	HP. No.5 feedwater heater outlet feedwater	Press.	P640	kg/cm <sup>2</sup> a	129,82
5		Temp.	T640,T641	°C	234,93
6		Enthalpy	$h_{fw}$	kcal/kg	242,46
7	No. 1 Extraction Steam	Press.	P110	kg/cm <sup>2</sup> a	34,38
8		Temp.	T110	°C	392,43
9		Enthalpy	$h_{E1}$	kcal/kg	766,24
10	No. 2 Extraction Steam	Press.	P120	kg/cm <sup>2</sup> a	18,05
11		Temp.	T120	°C	290,01
12		Enthalpy	$h_{E2}$	kcal/kg	718,47
13	No. 3 Extraction Steam	Press.	P130	kg/cm <sup>2</sup> a	8,43
14		Temp.	T130	°C	210,08
15		Enthalpy	$h_{E3}$	kcal/kg	683,46
16	HP. No.4 feedwater heater inlet feedwater	Press.	P620	kg/cm <sup>2</sup> a	172,32
17		Temp.	T620	°C	174,54
18		Enthalpy	$h_{w1}$	kcal/kg	178,57
19	HP. No.5 feedwater heater inlet feedwater	Press.	P620,P640	kg/cm <sup>2</sup> a	129,82
20		Temp.	T630	°C	201,00
21		Enthalpy	$h_{w2}$	kcal/kg	205,74
22	Deaerator outlet condensate	Press.	P600	kg/cm <sup>2</sup> a	6,17
23		Enthalpy	$h_{dea}$	kcal/kg	160,26
24	Deaerator Inlet Condensate	Temp.	T540	°C	134,17
25		Enthalpy	$h_{co}$	kcal/kg	134,76

26	HP No.4 feedwater heater drain	Press.	P120	kg/cm <sup>2</sup> a	18,05
27		Temp.	T625	°C	206,59
28		Enthalpy	$h_{d1}$	kcal/kg	668,04
29	HP No.5 feedwater heater drain	Press.	P110	kg/cm <sup>2</sup> a	34,38
30		Temp.	T635	°C	208,61
31		Enthalpy	$h_{d2}$	kcal/kg	213,01
32	Auxiliary steam before desuperheater	Press.	P810	kg/cm <sup>2</sup> a	18,14
33		Temp.	T800	°C	463,75
34		Enthalpy	$h_{sh}$	kcal/kg	810,00
35	Auxiliary steam after desuperheater	Press.	P810	kg/cm <sup>2</sup> a	18,14
36		Temp.	T810	°C	320,22
37		Enthalpy	$h_{ash}$	kcal/kg	734,76
38	Steam to Ejector	Press.	P810	kg/cm <sup>2</sup> a	18,14
39		Temp.	T810	°C	320,22
40		Enthalpy	$h_{ae}$	kcal/kg	734,76
41	Gland Seal Steam	Press.	P810	kg/cm <sup>2</sup> a	18,14
42		Temp.	T810	°C	320,22
43		Enthalpy	$h_{gl}$	kcal/kg	734,76
44	Make-up water	Temp.	T900	°C	35,54
45		Enthalpy	$h_{mu}$	kcal/kg	35,56
46	Spray from BFP	Press.	P620	kg/cm <sup>2</sup> a	172,32
47		Temp.	T620	°C	174,54
48		Enthalpy	$h_{sp}$	kcal/kg	178,57
49	SH Spray	Press.	P620	kg/cm <sup>2</sup> a	172,32
50		Temp.	T620	°C	174,54
51		Enthalpy	$h_{ss}$	kcal/kg	178,57

Catatan :

- Enthalpy dari Main Steam dihitung dari Main Steam Pressure dan Main Steam Temperature
- Enthalpy dari HP No.5 Feedwater Heater Drain dihitung dari No.1 Extraction Steam Pressure dan Drain Temperature.
- Enthalpy dari HP No.4 Feedwater Heater Drain dihitung dari No.2 Extraction Steam Pressure dan Drain Temperature.

- Data Atmospheric Pressure dari DCS digunakan untuk konversi dari tekanan terukur
- Semua data enthalphy dihitung dengan menggunakan software steam table Chemicallogic Steam Tab Companion.

## 2. 2. Data Pebanding 3 Febuari 2016 (Pembebanan 90%, 90 MW )

**TABEL 1.4 DATA TERUKUR PEBANDING**

Tanggal : 3 Febuari 2016

Durasi: 1 Jam

Beban : 91 MW

NO.	Measuring point No.	Tag Number	Measuring Point	Unit	90%
			KWH transfer awal	MWh	4.757.062,1
			KWH transfer akhir	MWh	4.759.004,7
			KWH UAT PS awal	MWh	85.940,3
			KWH UAT PS akhir	MWh	86.180,8
1	E300	4MKA10CE001XV1	Generator watthour	kWh	90.963
2	E301	4MKA10CE009XV1	Generator Active Power	kW	91.092
3	E302	4MKA10CE003XV1	Generator Voltage	kV	11.30
4	E303	4MKA10CE006XV1	Generator Current	kA	5.299,80
5	E304	4MKA10CE012XV1	Generator power factor	-	0,90
6	E305	4MKA10CE011XV1	Generator Frequency	Hz	50,30
7	E306	4CBA10CE009XV1	Field (excitation) DC Voltage	V	278,10
8	E307	4CBA10CE010XV1	Field (excitation) DC Current	A	764,40
9					
<b>FLOW</b>					
10	F520	4LCA30CF001XV1	LP No.1 Feedwater heater inlet condensate	t/h	321,50
11	F540	4LCA50CF001XV1	Dearator inlet condensate	t/h	313,40
12	F640	4HAC10CF001XV1	HP No.5 Feedwater heater outlet feedwater	t/h	276,20
13	F691	4LAE10CF001	SH1 Spray	t/h	17,60
14	F692	4LAE20CF001	SH2 Spray	t/h	22,80
15	F810	4LBG10CF001	Aux. Steam from SH after desuperheater	t/h	-
16	F900	4LCP62CF001XV1	Make-up water	t/h	8,20

PRESSURE					
18	P000	OQP10CP661	Atmospheric	hPa	1.008,34
19	P100	4LBA20CP010XV1	Main Steam	kg/cm <sup>2</sup> g	106,50
20	P105	4MAA10CP001XV1	Turbine Chamber	kg/cm <sup>2</sup> g	105,20
21	P110	4LBQ10CP001XV1	No. 1 Extraction Steam	kg/cm <sup>2</sup> g	30,90
22	P120	4LBQ20CP001XV1	No. 2 Extraction Steam	kg/cm <sup>2</sup> g	15,90
23	P130	4LBS30CP001	No. 3 Extraction Steam	kg/cm <sup>2</sup> g	6,70
24	P140	4LBS40CP001	No. 4 Extraction Steam	kg/cm <sup>2</sup> g	2,15
25	P150	4LBS50CP001	No. 5 Extraction Steam	kg/cm <sup>2</sup> g	(0,20)
26	P400	4MAG10CP011XV1	Turbine Exhaust	kg/cm <sup>2</sup> a	0,08
27	P510	4LCA20CP001XV1	Condensate Pump Discharge	kg/cm <sup>2</sup> g	15,43
28	P600	4LAA10CP001XV1	Deaerator Internal	kg/cm <sup>2</sup> g	4,20
29	P620	4LAB20CP001XV1	BFP discharge feedwater	kg/cm <sup>2</sup> g	172,40
30	P640	4HAC10CP001	HP No.5 Feedwater heater outlet feedwater	kg/cm <sup>2</sup> g	116,10
33	P800	4HAH72CP001	SH steam to HP aux. steam header	kg/cm <sup>2</sup> g	111,50
34	P810	4LBG10CP001	SH steam to HP aux. steam after desuperheater	kg/cm <sup>2</sup> g	17,40

**TABEL 1.5 DATA TEMPERATURE TERUKUR PEBANDING**

NO.	Measuring point No.		Measuring Point	Unit	100%
TEMPERATURE					
36	T000	LOCAL	Ambient	°C	
37	T100	4LBA20CT003XV1	Main Steam	°C	535,50
38	T101	4LBA20CT001XV1	Main Steam (LOT3)	°C	536,90
39	T110	4LBQ10CT001XV1	No. 1 extraction steam	°C	395,30
40	T120	4LBQ20CT001XV1	No. 2 extraction steam	°C	292,30
41	T130	4LBS30CT001	No. 3 extraction steam	°C	211,30
42	T400	4MAG10CT001	Turbine exhaust	°C	41,10
43	T480	4PAB50CT001XV1	Condenser Inlet cooling water A	°C	30,80

44	T481	4PAB60CT001XV1	Condenser Inlet cooling water B	°C	30,70
45	T490	4PAB51CT001XV1	Condenser outlet cooling water A	°C	37,60
46	T491	4PAB61CT001XV1	Condenser outlet cooling water B	°C	37,70
47	T500	4LCA10CT001XV1	Condenser outlet condensate	°C	43,20
48	T525	4LCJ10CT001XV1	LP No. 1 feedwater heater drain	°C	52,00
49	T530	4LCA40CT001XV1	LP No. 2 feedwater heater inlet condensate	°C	90,70
50	T535	4LCJ20CT001XV1	LP No. 2 feedwater heater drain	°C	97,00
51	T540	4LCA50CT001XV1	Deaerator Inlet Condensate	°C	130,70
52	T600	4LAA10CT001XV1	Deaerator Internal	°C	167,70
53	T620	4LAB20CT001XV1	BFP discharge feedwater	°C	171,30
54	T625	4LCH40CT001XV1	HP No. 4 feedwater heater drain	°C	202,20
55	T630	4LAB30CT001XV1	HP No. 5 feedwater heater inlet feedwater	°C	198,00
56	T635	4LCH50CT001XV1	HP No. 5 feedwater drain	°C	203,10
57	T640	4LAB40CT001XV1	HP No. 5 feedwater heater outlet feedwater 1	°C	230,60
58	T641	4HAC10CT001	HP No. 5 feedwater heater outlet feedwater 2	°C	231,80
59	T800	4HAH72CT002XV1	SH steam to HP aux. steam header	°C	465,90
60	T810	4LBG10CT001	SH steam to HP aux. steam after desuperheater	°C	329,70
61	T900	4LCP11CT001XV1	Make-up water	°C	29,20

**TABEL 1.6 PERHITNGAN ENTHALPHI PEBANDING**

Tanggal : 3 Febuari 2016

Durasi : 1 Jam

Beban : 91 MW

No.	ITEM	SYMBOL	UNIT	90%	
1	Main Steam	Press.	P100	kg/cm <sup>2</sup> a	107,53
2		Temp.	T100,T101	°C	535,50
3		Enthalpy	$h_{ms}$	kcal/kg	825,90
4	HP. No.5 feedwater heater outlet feedwater	Press.	P640	kg/cm <sup>2</sup> a	117,13
5		Temp.	T640,T641	°C	230,60
6		Enthalpy	$h_{fw}$	kcal/kg	242,93
7	No. 1 Extraction Steam	Press.	P110	kg/cm <sup>2</sup> a	31,93
8		Temp.	T110	°C	395,30
9		Enthalpy	$h_{E1}$	kcal/kg	764,63

10	No. 2 Extraction Steam	Press.	P120	kg/cm <sup>2</sup> a	16,93
11		Temp.	T120	°C	292,30
12		Enthalpy	h <sub>E2</sub>	kcal/kg	717,61
13	No. 3 Extraction Steam	Press.	P130	kg/cm <sup>2</sup> a	7,73
14		Temp.	T130	°C	211,30
15		Enthalpy	h <sub>E3</sub>	kcal/kg	680,76
16	HP. No.4 feedwater heater inlet feedwater	Press.	P620	kg/cm <sup>2</sup> a	173,43
17		Temp.	T620	°C	171,30
18		Enthalpy	h <sub>w1</sub>	kcal/kg	177,89
19	HP. No.5 feedwater heater inlet feedwater	Press.	P620,P640	kg/cm <sup>2</sup> a	117,13
20		Temp.	T630	°C	198,00
21		Enthalpy	h <sub>w2</sub>	kcal/kg	204,40
22	Deaerator outlet condensate	Press.	P600	kg/cm <sup>2</sup> a	5,23
23		Enthalpy	h <sub>dea</sub>	kcal/kg	173,30
24	Deaerator Inlet Condensate	Temp.	T540	°C	130,70
25		Enthalpy	h <sub>co</sub>	kcal/kg	134,53
26	HP No.4 feedwater heater drain	Press.	P120	kg/cm <sup>2</sup> a	16,93
27		Temp.	T625	°C	202,20
28		Enthalpy	h <sub>d1</sub>	kcal/kg	181,46
29	HP No.5 feedwater heater drain	Press.	P110	kg/cm <sup>2</sup> a	31,93
30		Temp.	T635	°C	203,10
31		Enthalpy	h <sub>d2</sub>	kcal/kg	213,29
32	Auxiliary steam before desuperheater	Press.	P810	kg/cm <sup>2</sup> a	18,43
33		Temp.	T800	°C	465,90
34		Enthalpy	h <sub>sh</sub>	kcal/kg	812,00
35	Auxiliary steam after desuperheater	Press.	P810	kg/cm <sup>2</sup> a	18,43
36		Temp.	T810	°C	329,70
37		Enthalpy	h <sub>ash</sub>	kcal/kg	729,20
38	Steam to Ejector	Press.	P810	kg/cm <sup>2</sup> a	18,43
39		Temp.	T810	°C	329,70
40		Enthalpy	h <sub>ae</sub>	kcal/kg	72,20
41	Gland Seal Steam	Press.	P810	kg/cm <sup>2</sup> a	18,43
42		Temp.	T810	°C	329,70
43		Enthalpy	h <sub>gl</sub>	kcal/kg	729,20
44	Make-up water	Temp.	T900	°C	29,20

45		Enthalpy	$h_{mu}$	kcal/kg	35,65
46	Spray from BFP	Press.	P620	kg/cm <sup>2</sup> a	173,43
47		Temp.	T620	°C	171,30
48		Enthalpy	$h_{sp}$	kcal/kg	177,89
49	SH Spray	Press.	P620	kg/cm <sup>2</sup> a	173,43
50		Temp.	T620	°C	171,30
51		Enthalpy	$h_{ss}$	kcal/kg	177,89

Catatan :

- Enthalpy dari Main Steam dihitung dari Main Steam Pressure dan Main Steam Temperature
- Enthalpy dari HP No.5 Feedwater Heater Drain dihitung dari No.1 Extraction Steam Pressure dan Drain Temperature.
- Enthalpy dari HP No.4 Feedwater Heater Drain dihitung dari No.2 Extraction Steam Pressure dan Drain Temperature.
- Data Atmospheric Pressure dari DCS digunakan untuk konversi dari tekanan terukur
- Semua data enthalpy dihitung dengan menggunakan software steam table Chemicallogic Steam Tab Companion.

### Data Logsheet Generator

#### 3. Data 1 Oktober 2014 (Pembebanan 100%, 100 MW )

**TABEL 1.7 DATA TERUKUR LOGSHEET GENERATOR**

TIME	LOAD (MW)				TEG	FREQ
	BRUTO	UAT	NETTO	MVAR	150 Kv	Hz
00.00	97,3	11,1	86,2	12	151	49,9
00.30	97,7	11,2	86,5	8,7	151,2	50,3
01.00	97,1	11,1	86	13,2	150,3	50,3
01.30	98,4	10,8	87,6	24,3	149,2	50,2
02.00	98,3	10,6	87,7	24,2	50,9	49,7
02.30	98,5	10,8	87,7	18,5	50,2	49,9
03.00	97,9	10,8	87,1	18,6	150,9	49,7
03.30	98,7	11,1	87,5	13,41	150,9	50,2
04.00	97,7	11	86,7	16,5	150,5	50,2
04.30	97,6	10,7	86,8	24,2	149,6	50
05.00	97,3	10,8	86,6	16,8	150,5	49,7

05.30	97,4	10,6	86,8	30,8	148,9	49,9
06.00	98,9	10,8	88	33,5	148,5	50,3
06.30	100,3	10,9	89,4	26,1	149,5	50,1
07.00	100,1	10,9	89,2	14,7	151	50
07.30	99,3	10	88,3	11,2	151,3	50
08.00	99,7	11,1	88,6	15,9	150,9	50
08.30	98,9	10,9	88,1	20,9	150,2	49,9
09.00	99,3	10,7	88,8	24,2	149,8	49,9
09.30	100	10,7	90,8	28,1	149,4	49,8
10.00	99,9	10,9	89	29,7	149,3	50,1
10.30	98,8	10,7	88,2	37,9	148,3	50,3
11.00	97,8	10,5	87,3	40,8	147,8	50
11.30	98	10,6	87,4	37,8	148,2	50,1
12.00	98,7	10,6	88	35,3	148,6	50,4
12.30	99,3	10,4	88,9	38,2	148,1	49,9
13.00	99,6	10,5	89,1	41,4	148	49,8
13.30	99,9	10,6	89,3	48,4	147,2	50,3
14.00	99,6	10,5	89,1	41,6	146	50,1
14.30	99,8	10,6	89,2	34,4	147	49,5
15.00	99,3	10,5	89,1	34,1	149	50,1
15.30	99,8	10,5	89,3	48,4	148	50,1
16.00	99,9	10,5	88	41,4	149	50,3
16.30	96,2	10,7	87,2	47,4	147,7	50,3
17.00	99,8	10,8	89	32,9	148,7	50,2
17.30	98	10,7	87,3	37	148,1	50
18.00	96	10,3	85,7	51,6	146,8	49,7
18.30	97,6	10,4	87,2	44,8	147,2	50,3
19.00	96,6	10,4	86,2	50,2	146,7	50,3
19.30	96,2	10,3	86,3	47,4	147	50,3
20.00	95,3	10,4	84,9	43,9	147,6	49,9
20.30	100,1	10,4	89,7	46	147	49,7
21.00	99,7	10,5	89,3	41	147,7	49,7
21.30	100	10,9	89,1	34,3	148,6	50,3
22.00	98,1	10,7	87,5	30,5	149,1	49,7
22.30	93,4	10,7	87,3	33	148,6	49,7
23.00	98,4	10,2	87,2	20,1	150,1	50,4

23.30	100,3	10,1	84,2	12,2	151	50,1
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Stand MWH meter (panel) Pukul 10.00

	EXPORT		IMPORT		UAT	
	MWH	MVARH	MWH	MVARH	MWH	MVARH
Hari ini	3.980.097,60	298.730,20	27.981,40	203.976,70	94.846,49	45.935,38
Kemarin	3.977.993,20	298.592,90	27.981,40	203.940,70	94.638,60	45.795,00
Hasil	2104,40	137,30		36	208,43	140,38

Tabel diatas menunjukkan nilai produksi, pemakaian maupun UAT PLTU Tarahan, lalu Total Pemakaian Batubara satu hari 24 jam yaitu 1.098 Ton adapun nilai produksi listrik nanti akan digunakan untuk perhitungan mencari nilai NPHR.

Catatan :

1Kcal : 4.186,8 J  
 1Kwh : 3.600.000 J  
 Nilai Kalori : 5.000 kcal

**1. Data Pebanding 3 Febuari 2016 (Pembebanan 90%, 90 MW )**

**TABEL 1.8 DATA TERUKUR LOGSHET GENERATOR PEBANDING**

TIME	LOAD (MW)				TEG	FREQ
	BRUTO	UAT	NETTO	MVAR	150 Kv	Hz
00.00	90	12,4	86,2	12	151,9	50,5
00.30	90,3	12,1	86,5	8,7	151,9	50,2
01.00	90,2	11,6	86	13,2	150,4	50,1
01.30	90,2	11,9	78,3	30,2	152,6	50,2
02.00	91,3	12	79,3	24,9	151,7	50,2
02.30	91,1	12,4	78,6	19,3	155,1	50,4
03.00	91,1	12,4	78,6	16	154	50,4
03.30	90,5	12,2	78,3	27,9	154,6	50,3
04.00	90,7	12,3	78,4	23,4	153,8	50,1
04.30	89,8	12,2	77,6	26,4	150,8	50,3
05.00	89,4	11,4	78	46	152,8	49,9
05.30	90,3	12,2	78,1	28,7	150,4	50,5
06.00	90,5	11,5	79	42,1	151	50,1
06.30	90,8	11,7	79	40,6	151,8	50,3

07.00	90,5	12,2	78,3	31,7	151,9	50,4
07.30	89,3	11,8	77,5	33,5	150,5	50,1
08.00	89,6	11,5	78,1	37,9	149,4	50,1
08.30	90,1	11,3	77,8	47,3	151,7	50,1
09.00	90,3	11,6	78,7	44,5	150,8	49,9
09.30	91,3	11,8	79,5	45,2	150,8	50,2
10.00	92	12	79,5	34,8	152,4	50,2
10.30	90,2	11,6	78	36,5	152,2	50,4
11.00	91,1	11,2	78,8	35,3	150,7	50,2
11.30	89,9	11,8	78,1	37,6	151	49,9
12.00	90,6	12	78,6	32,8	150,4	50,2
12.30	90	11,6	78,4	39,2	150,5	50,2
13.00	91,6	11,2	80,4	44,8	149	50,2
13.30	92,3	11,7	80,6	43,4	148,4	50,3
14.00	92,2	12	80,2	43,4	150	50,3
14.30	92,5	11,6	81	40	149,1	50,3
15.00	91,3	11,6	79,7	44,5	151,3	50,3
15.30	92	11,4	80,6	38,3	150	50,2
16.00	91,4	11,8	79,6	43,3	150,5	50,3
16.30	91,4	11,9	79,5	40,3	150,5	49,9
17.00	91,7	11,9	79,8	41,9	151,5	50,4
17.30	91,6	12,6	79	41,9	151,2	50,2
18.00	91,4	12	79,4	31,5	150,2	49,8
18.30	91,7	11,8	80	29,2	152	50,2
19.00	91,6	12,2	79,4	35,9	152,4	50,4
19.30	91,6	12,7	78,9	23,9	152,4	50,4
20.00	91,4	12,5	78,9	22,5	152,4	50,1
20.30	91,4	12,6	78,9	23,4	151,6	50,1
21.00	92,8	12,6	80,2	27,8	153	50,1
21.30	92,7	12,1	80,6	25,3	152,8	49,9
22.00	92,4	12,4	80,2	29,3	152,8	50,2
22.30	93,5	12,7	80,9	26,8	155,5	50,2
23.00	92,4	12,6	79,8	22,2	154,2	50,1
23.30	93,5	12,5	81	81	155,1	49,8

	EXPORT		IMPORT		UAT	
	MWH	MVARH	MWH	MVARH	MWH	MVARH
Hari ini	4.759.004,7	410.072,8	31.546,7	217.803,7	86.180,8	8.085,9
Kemarin	4.757.062,1	409.557	31.546,7	217.803,6	85.940,3	7.923,9
Hasil	1.942,6	515,8	0	0,1	240,5	162,03

Tabel diatas menunjukkan nilai produksi, pemakaian maupun UAT PLTU Tarahan, lalu Total Pemakaian Batubara satu hari 24 jam yaitu 1.098 Ton adapun nilai produksi listrik nanti akan digunakan untuk perhitungan mencari nilai NPHR.

Catatan :

1Kcal : 4.186,8 J

1Kwh : 3.600.000 J